



China Australia Geological Storage of CO₂
中澳二氧化碳地质封存



清华大学

The Studies on Environmental Impact and Risk Management of CO₂ Storage

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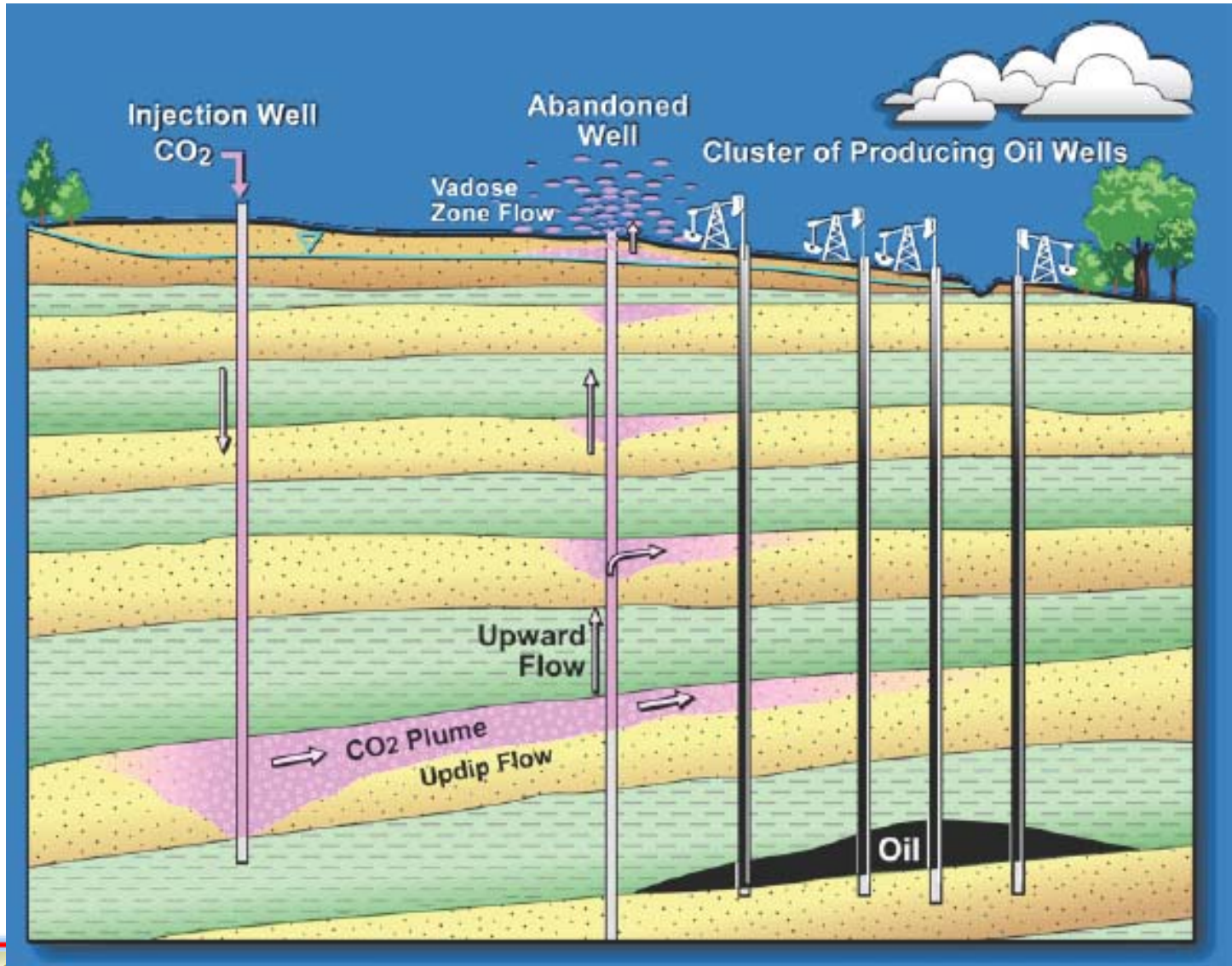
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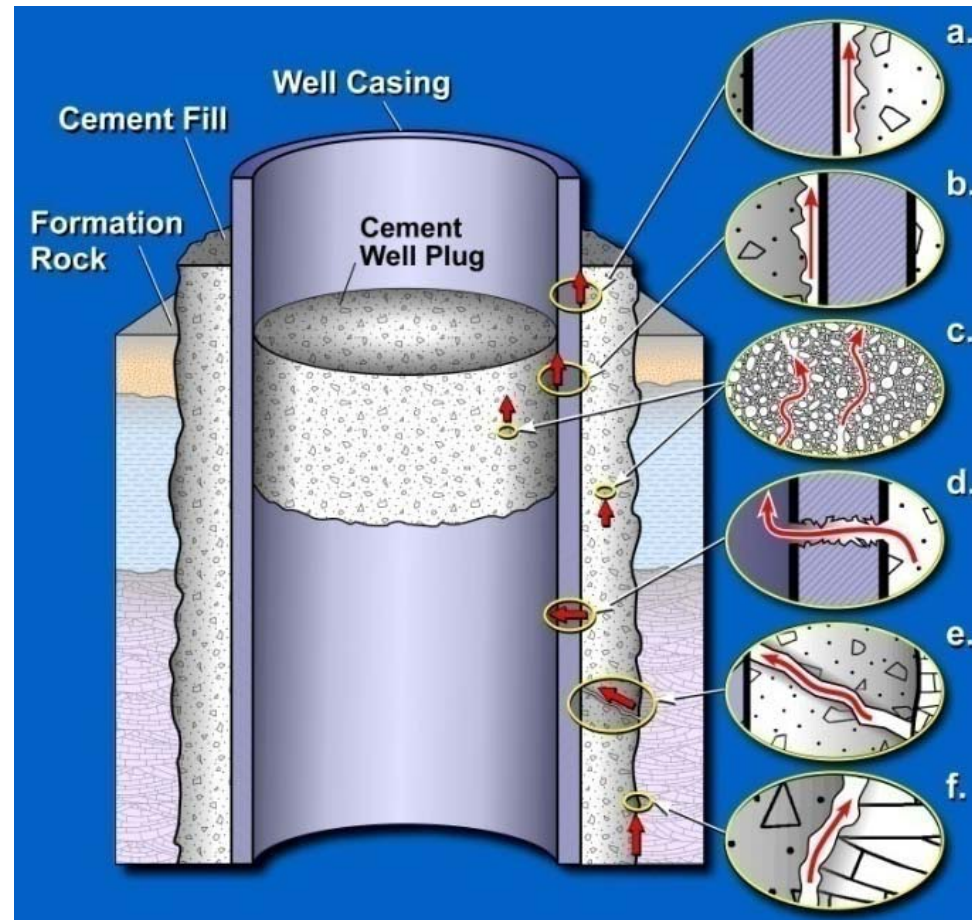
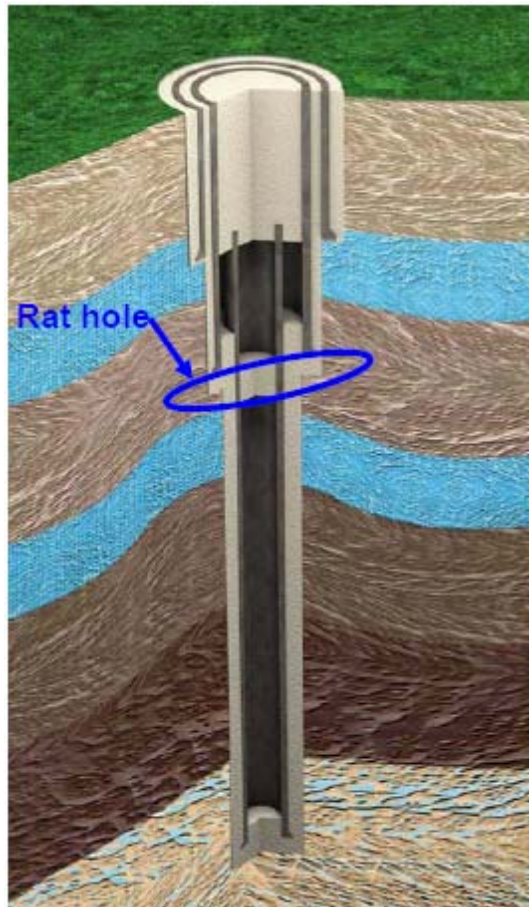
Main works



- **Case Study: Numerical Simulation on Leakage of Injected CO₂ into Overlying Formations through a Leaky Well** 针对封存场地中已有废弃井的情况，通过数值模拟方法，研究了**废弃井对CO₂地质封存泄露的影响**。
 - Develop the simulation method 提出并发展了**新的数值模拟方法**；
 - Quantities analysis on leakage ratio, Maximum leakage ratio **time**, leakage rate various with time, etc. **定量分析了泄漏量随时间的变化**，初步分析了**相关因素对泄漏的影响**；
 - Provide technical and data support to risk assessment 为CO₂封存风险研究提供了**技术和数据支持**。

1.1 Leakage through a Leaky Well





Problem 1: CO₂ leakage risk

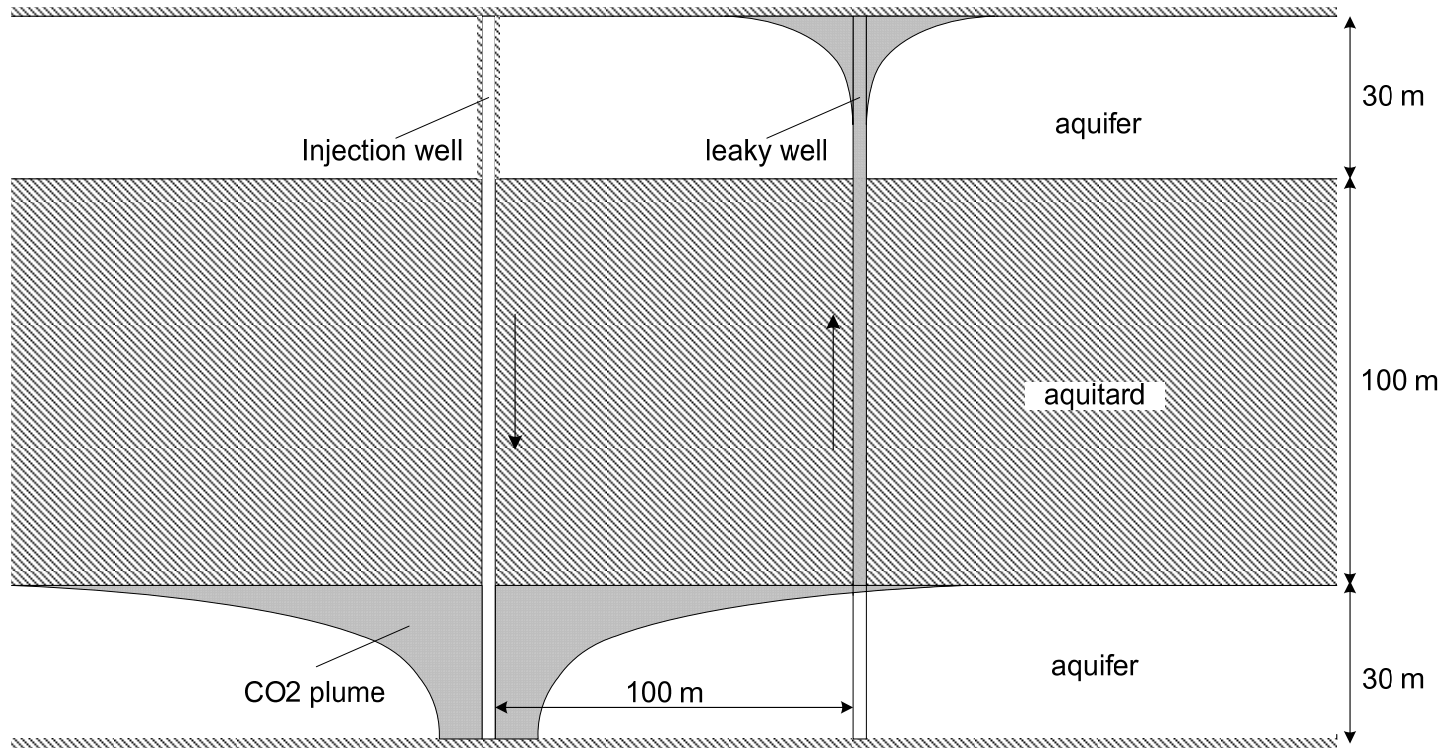


Figure Leakage scenario

CO₂ is injected into the **deeper aquifer**, spreads within the deeper aquifer and upon reaching the **leaky well**, rises up to the **shallower aquifer**.

Problem 1: Governing equations



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Simulated by commercial software **FLUENT 6.3** code,
Multi-phase model: **Eulerian Model** .

Continuity equation:

$$\frac{\partial(\varphi S_i \rho_i)}{\partial t} + \nabla \cdot (\varphi S_i \rho_i \bar{v}_i) = 0, \quad (i = w, g)$$

where φ is the **porosity**; S_i is the **saturation** of phase i ; ρ_i is **the density** of phase i ; \bar{v}_i is **the velocity** vector of phase i .

Momentum equation:

$$\frac{\partial(\varphi S_i \rho_i \bar{v}_i)}{\partial t} + \nabla \cdot (\varphi S_i \rho_i \bar{v}_i \bar{v}_i) = -\varphi S_i \nabla P + \nabla \cdot \left[\varphi S_i \mu_i \left(\nabla \bar{v}_i + \bar{v}_i^T - \frac{2}{3} \nabla \cdot \bar{v}_i \mathbf{I} \right) \right] + \varphi S_i \rho_i \bar{g} - S_i \frac{\mu_i}{k_{r,i}} \bar{v}_i$$

Where P is **pressure**, \mathbf{I} is the unit **tensor**, μ_i is the **viscosity** of phase, \bar{g} is the **gravity** vector, $k_{r,i}$ is **relative permeability**, and K is the **absolute permeability** tensor.

Problem 1: model parameters

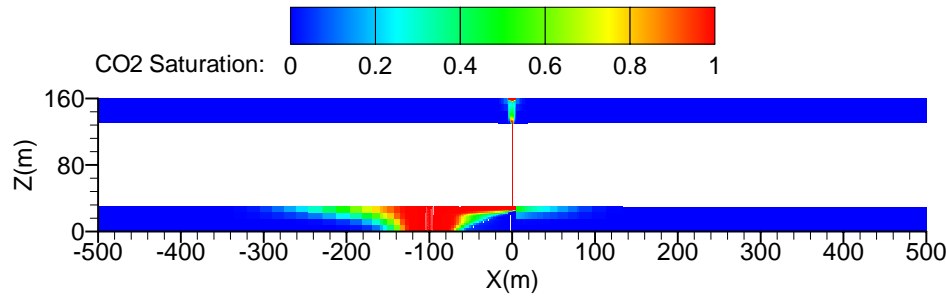


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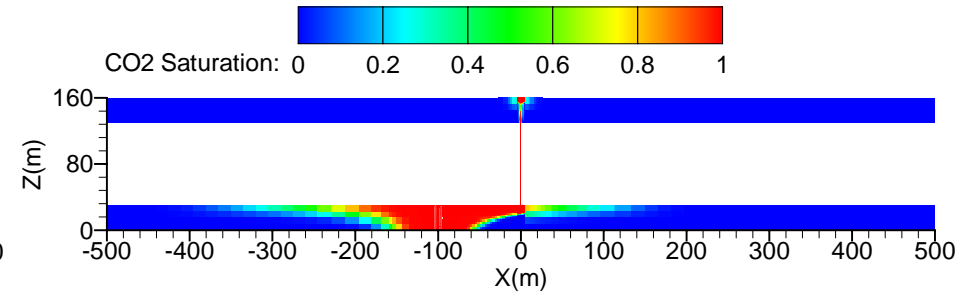
Parameter	Value
Dimensions of the model domain	1000 m × 1000 m × 160 m
Aquifer depth	2840 - 3000 m
Aquifer thickness	30 m
Aquitard thickness	100 m
Porosity	0.15
Radius of leaky and injection wells	0.15 m
Distance between wells	100 m
Aquifer permeability	$2 \times 10^{-14} \text{ m}^2$
Leaky well permeability	$1 \times 10^{-12} \text{ m}^2$
Relative permeability	linear
Initial brine saturation	100%
Initial pressure distribution	Hydrostatic, gradient of 10251.145 Pa/m
CO ₂ density	$(k_{r,i} = S_i)$ 479 kg/m ³
Brine density	1045 kg/m ³
CO ₂ viscosity	$3.950 \times 10^{-5} \text{ Pas}$
Brine viscosity	$2.535 \times 10^{-4} \text{ Pas}$
CO ₂ injection rate	8.87 kg/s
Simulation time	1000 days

- Lateral boundary conditions: kept constant identical to the initial conditions;
- Boundaries at the top and bottom of the two aquifers no-flow boundaries;
- All processes are isothermal;
- none of the boundary changes over time.

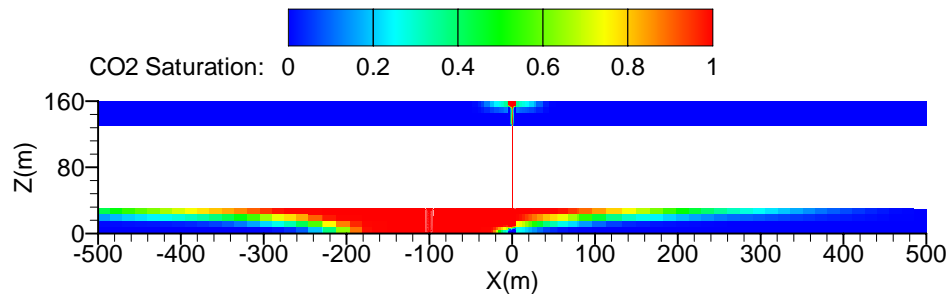
Problem 1: Results (1)



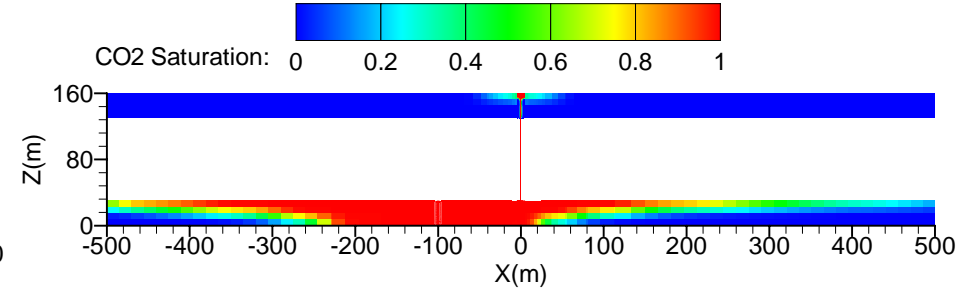
a) after 60 days of CO₂ injection



b) after 115 days of CO₂ injection



c) after 520 days of CO₂ injection



d) after 1000 days of CO₂ injection

Figure Distribution CO₂ saturation on the vertical middle slice

Injected CO₂ **spreads in the radial direction** from the injection location, comes in contact with the leaky well and rises to the shallower aquifer.

Problem 1: Results (2)

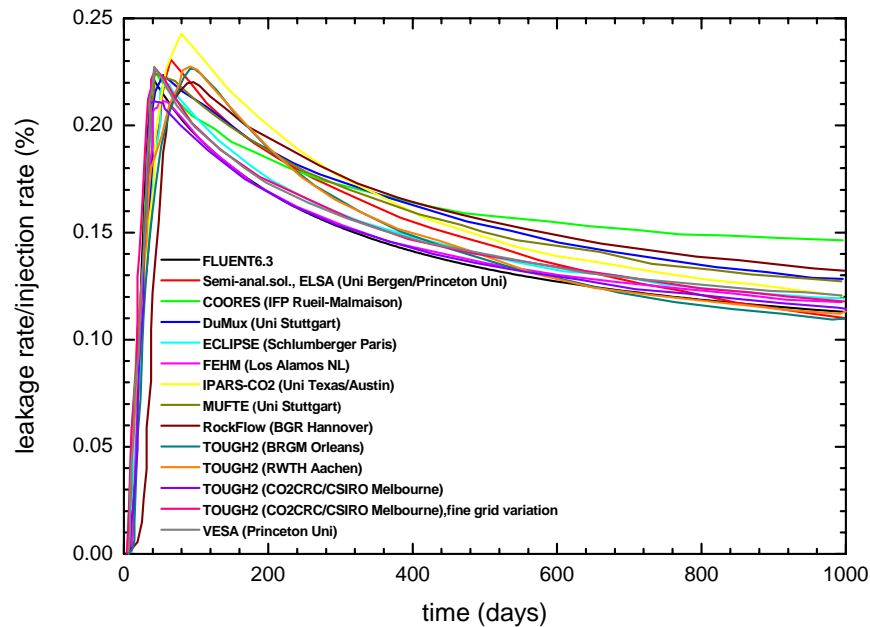


Figure Comparison of predicted CO₂ leakage ratio values over time obtained by different codes

leakage ratio

(ratio of leakage rate to injection rate)

- **Maximum** CO₂ leakage ratio;
- Maximum leakage ratio **time**;
- Leakage ratio **after 1000 days** of injection;
- **CO₂ arrival time** at the leaky well (leakage ratio is larger than $5.0 \times 10^{-3} \%$).

Table Comparison of some interesting values computed by different codes

Code	Max. leakage (%)	Time at max. leakage (days)	Leakage at 1000 days (%)	Arrival time (days)
FLUENT 6.3	0.221	42	0.113	10
ELSA (Semi-analytical solution) (Uni Bergen/Princeton Uni)	0.231	63	0.109	14
COORES (IFP)	0.219	50	0.146	8
DuMux (Uni Stuttgart)	0.220	61	0.128	6
ECLIPSE (Schlumberger)	0.225	48	0.118	8
FEHM (Los Alamos NL)	0.216	53	0.119	4
IPARS-CO2 (Uni Texas/Austin)	0.243	80	0.120	10
MUFTE (Uni Stuttgart)	0.222	58	0.126	8
RockFlow (BGR)	0.220	74	0.132	19
TOUGH2/ECO2N (BRGM)	0.226	93	0.110	4
TOUGH2/ECO2N (refined grid) (CO2CRC/CSIRO)	0.212 0.225	46 45	0.115 -	10 8
TOUGH2 (RWTH Aachen)	0.227	89	0.112	9
VESA (Princeton Uni)	0.227	41	0.120	7

Problem 1: results(3)



Non-linear relative permeability:

$$\begin{cases} k_{w,r} = S_e^4 \\ k_{g,r} = (1 - S_e)^2 \cdot (1 - S_e^2) \end{cases} \quad \& \quad S_e = \frac{S_w - S_{w,R}}{1 - S_{w,R} - S_{g,R}}$$

S_e is **effective saturation**;

$S_{w,R}$ is the **residual brine saturation**;

$S_{g,R}$ is the **residual gas saturation**.

Non-linear relative permeability:

- **increases overall resistance**;
 - **enhances** the influence of **viscous** force;
 - **weakens** the **buoyancy** driven force;
- these make the CO₂ front shape **more cylindrical** than linear rela.perm. case.

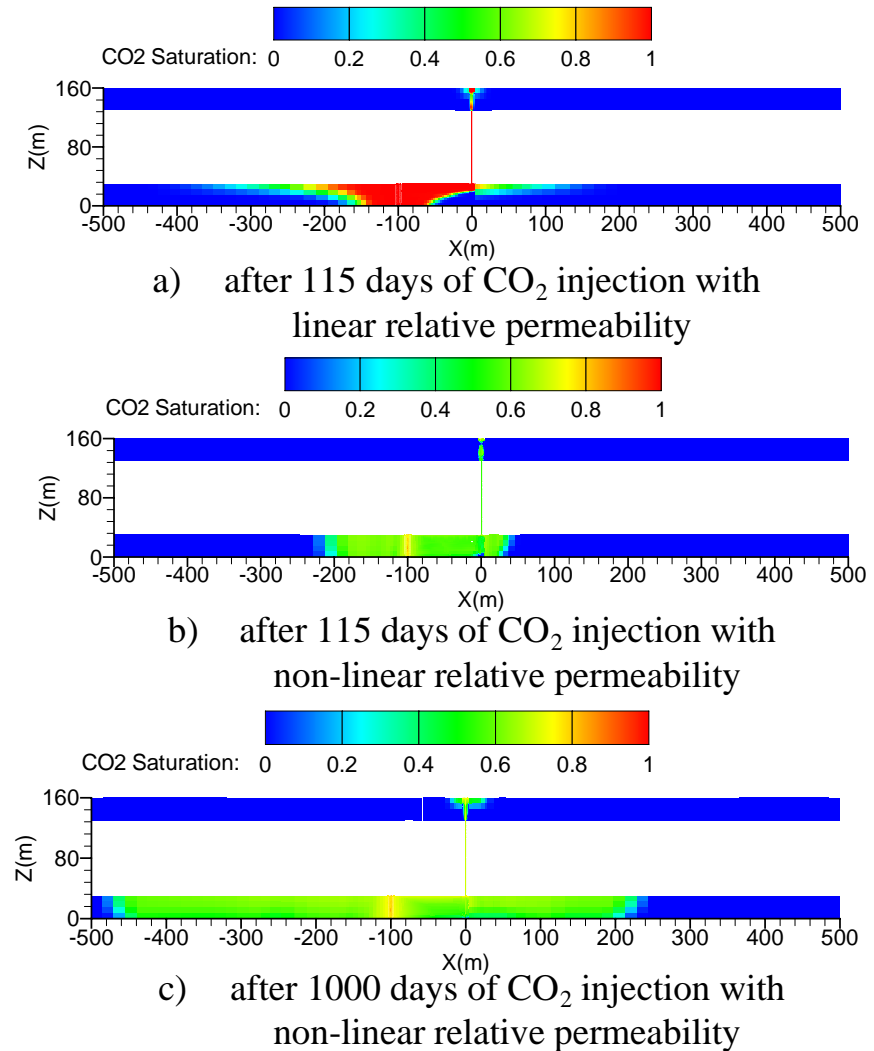


Figure Distribution CO₂ saturation on the vertical middle slice

Problem 1: results(4)



Non-linear relative permeability:

$$\begin{cases} k_{w,r} = S_e^4 \\ k_{g,r} = (1 - S_e)^2 \cdot (1 - S_e^2) \end{cases} \quad \& \quad S_e = \frac{S_w - S_{w,R}}{1 - S_{w,R} - S_{g,R}}$$

- S_e is effective saturation;
- $S_{w,R}$ is the residual brine saturation;
- $S_{g,R}$ is the residual gas saturation.

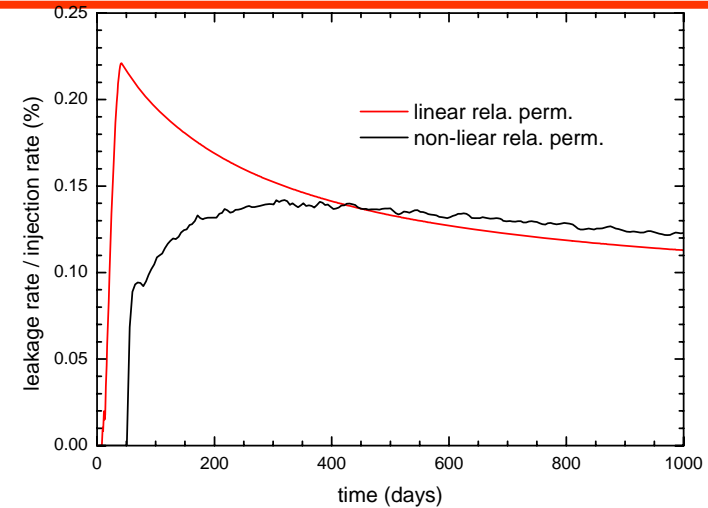


Figure Predicted CO₂ leakage ratio values over time with linear relative permeability-saturation or non-linear relative permeability-saturation

Table Computed results with different relative permeability relations

Case	Max. leakage (%)	Time at max. leakage (days)	Leakage at 1000 days (%)	Arrival time (days)
Linear relative permeability-saturation	0.221	43	0.113	9
Non-linear relative permeability-saturation	0.142	307	0.123	52

Non-linear relative :

- decelerates CO₂ arrival time;
- lowers the maximum leakage rate;
- lowers leakage rate in the early period;
- improves leakage rate in the late period.